Natural Refrigerant Training Summit

Building a Sustainable Workforce

CO2 Transcritical Compressors: Design, Lab Testing, and Troubleshooting

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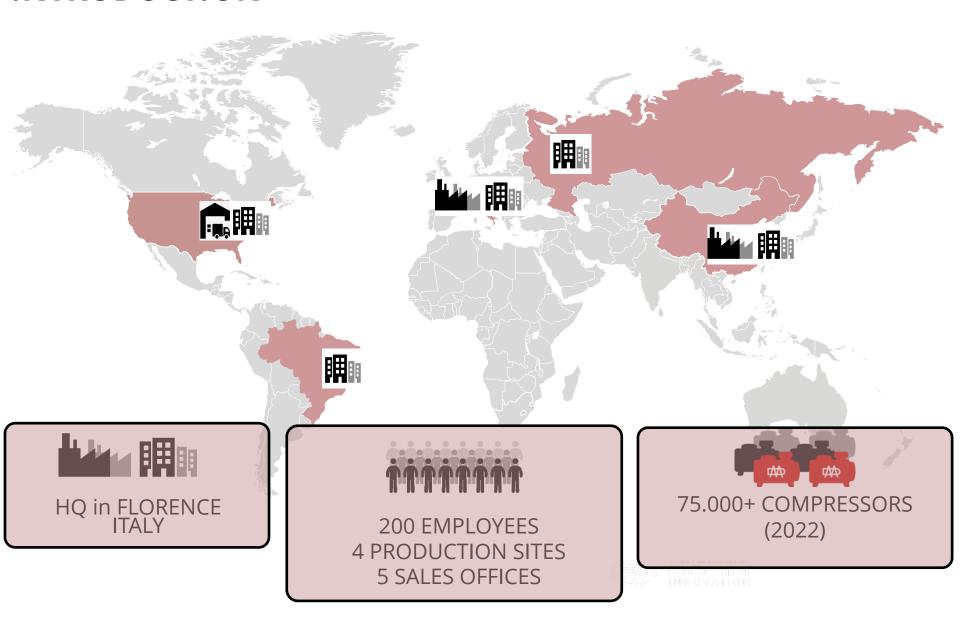




CO₂ TRANSCRITICAL COMPRESSORS: DESIGN - LAB TESTING - TROUBLESHOOTING



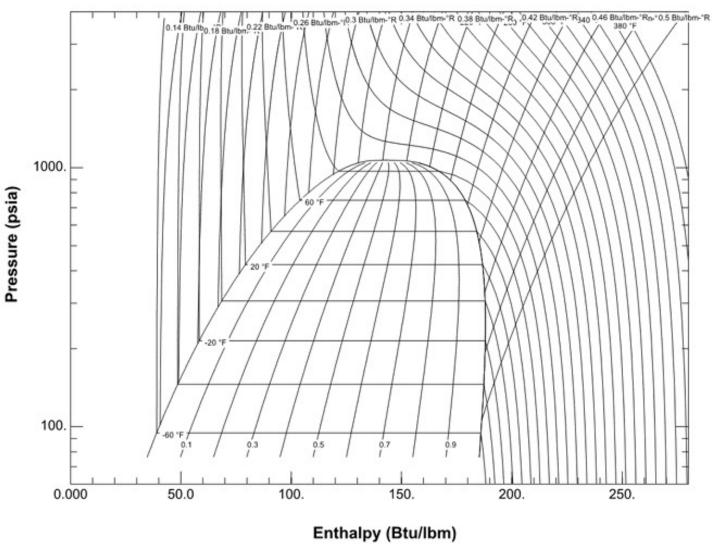
INTRODUCTION



Introduction to CO2

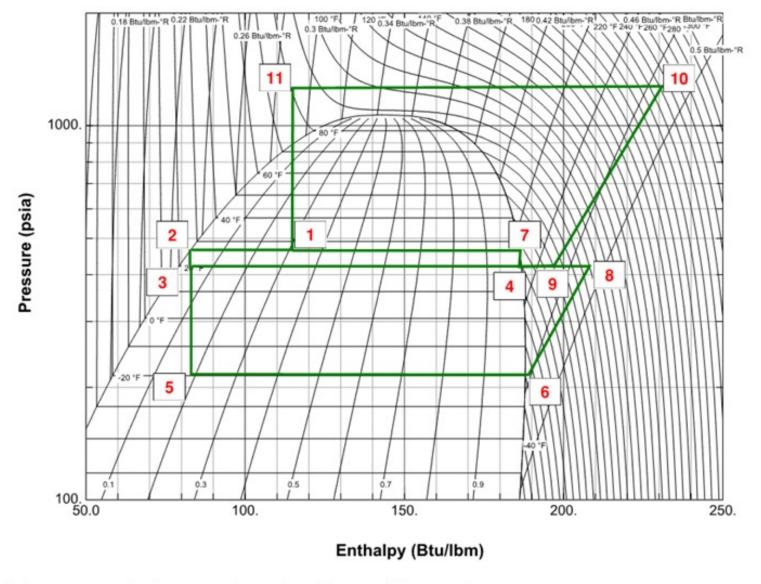
- Carbon Dioxide (R744 CO2)
- Environmentally benign properties (GWP = 1)
- Excellent heat transfer properties
- High COP levels
- Severe challenges from a compressor perspective
- Important Conditions to remember:
 - Critical Point = 1070psia / 87.8F
 - Triple Point = 75psia / -69.8F
 - Low Temp Evap Operation = ~180psig / -25F
 - Med Temp Evap Operation = ~400psig / +20F
 - Condensing = 1031.5psig / 86F
- Design and Test criteria for a 4412 cfh 160hp CO2 transcritical compressor analyzed over the course of this training.

CO2 PH Diagram



^{*} Diagram created using REFPROP - NIST Reference Fluid Properties

CO2 Flash Gas Bypass System



^{*} Diagram created using REFPROP - NIST Reference Fluid Properties

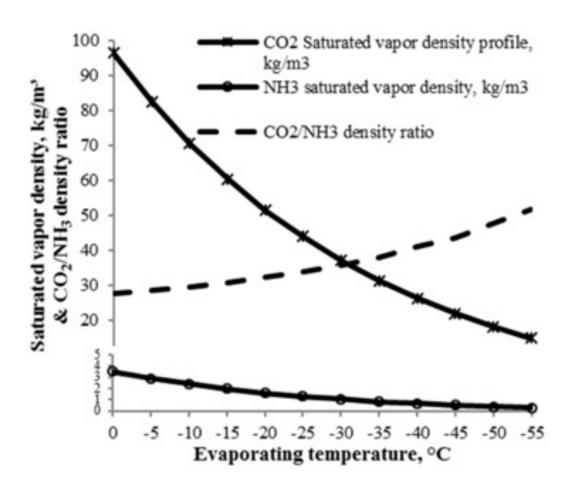


Pressure Differential – Medium Temperature Systems

MT SYSTEM OPERATION							
-10°C (14°F) SST // 40°C (104°F) AMB. TEMP.	R404A	R134a	R449A	NH ₃	CO ₂		
Differential Pressure [bar]	18,6	11,2	17,7	17,4	73,5		
Differential Pressure [psi]	270	162,4	256,6	252,3	1066		

- CO2 has a pressure differential up to 6.5x higher than other refrigerants
- Reciprocating technology best deals with this high pressure differential
- There still remains severe challenges for drive gear design

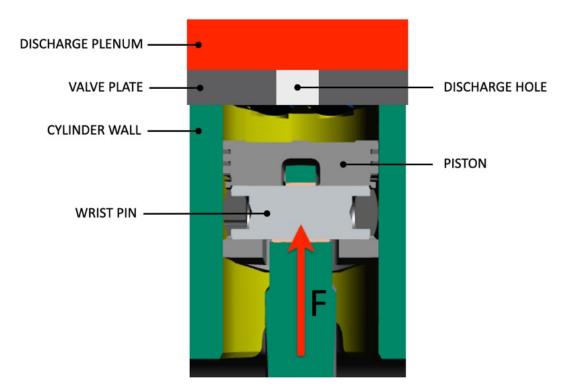
Volumetric Refrigeration Capacity



- CO2 has a very high volumetric refrigeration capacity
- 4~12 times larger than NH3
- Similar capacity using smaller displacements
- Much smaller pipe diameters
- Much smaller compressor bores

- Less room to unload compressor stresses
- Very high specific load on the drive gear

Specific Load on the Drive Gear



- CO2 induces a very high specific load on the drive gear due to large differential pressures and small bores.
- Wrist Pin is the most challenged component
- p = F / A (wrist pin specific load)
- $F = \Delta p * piston top surface$
- A = contact surface between rod end and wrist pin

Specific Load on the Drive Gear – Medium Temperature Systems

MT SYSTEM OPERATION	-10°C (14°F) SST	// 40°C (104	°F) AMB. TE	MP.	
140 kW [480 kBtu/h] refrigeration duty	R404A	R134a	R449A	NH ₃	CO2
displacement @ 1750 rpm [m3/h]	300	500	300	300	75
displacement @ 1750 rpm [cfh]	10560	17640	10560	10560	2640
number of cylinders	8	12	8	8	6
bore [mm]	86	95	86	86	55
bore [inches]	3,38	3,74	3,38	3,38	2,16
force [N]	1,02E+04	7,44E+03	9,53E+03	1,01E+04	1,75E+04
wrist pin contact surface [mm2]	9,42E+02	1,02E+03	9,42E+02	9,42E+02	5,09E+02
wrist pin specific load [MPa]	10,8	7,29	10,1	10,7	34,3

CO2 induces:

- ~3x the specific load of NH3, R404A and R449A.
- ~5x the specific load of R134A.

High Discharge Temperatures – Medium Temperature Systems

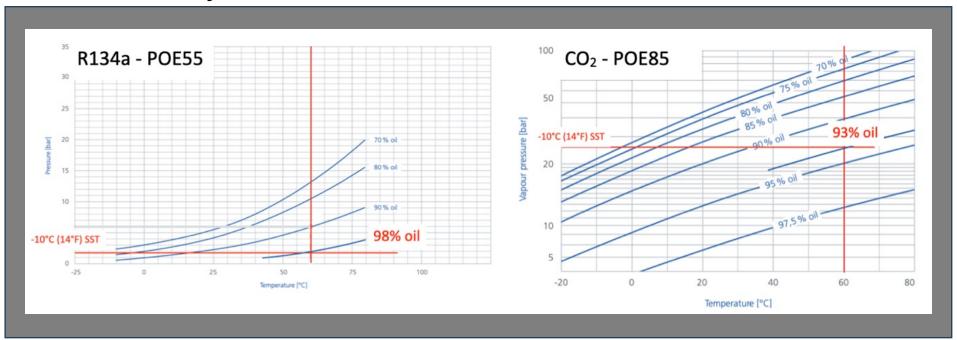
MT SYSTEM OPERATION -10°C (14°F) SST // 40°C (104°F) AMB. TEMP. // 30K (54F) SUPERHEAT						
Refrigerant	R404A	R134a	R449A	NH ₃	CO ₂	
polytropic exponent	1,004830	1,070567	NA	1,320000	1,289373	
RDT [°C]	91,3	96,2	99,5	out of envelope	155	
RDT [°F]	196	205	211	out of envelope	311	

Table 4. Real discharge temperatures for various MT refrigerants systems

CO2 leads to significantly higher discharge temperatures – challenges:

- Heat Dissipation
- Lubrication

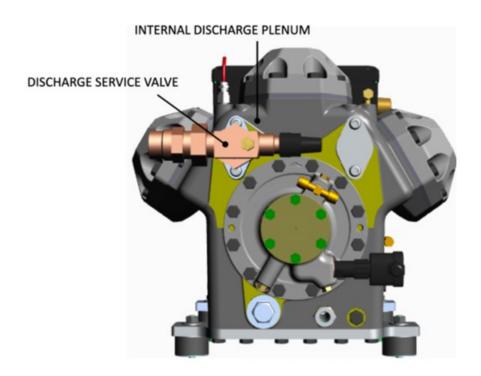
CO2 Solubility in Lubricants

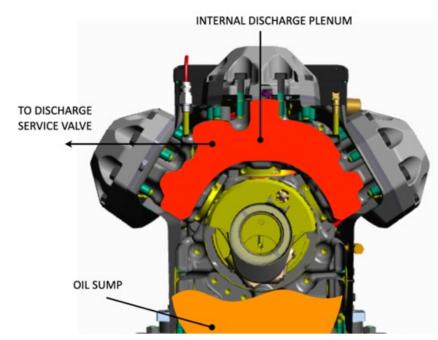


CO2 is more soluble into lubricants – challenges:

- Lower residual viscosity
- Higher oil circulation rate

DESIGN A





Internal Discharge Plenum:

- Crank-case material Cast Iron (thermal conductor)
- Compression heat dissipates towards the lubricant

DESIGN B



Figure 7. Design B - compressor with external discharge plenum

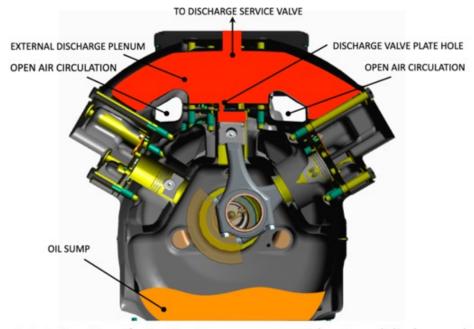
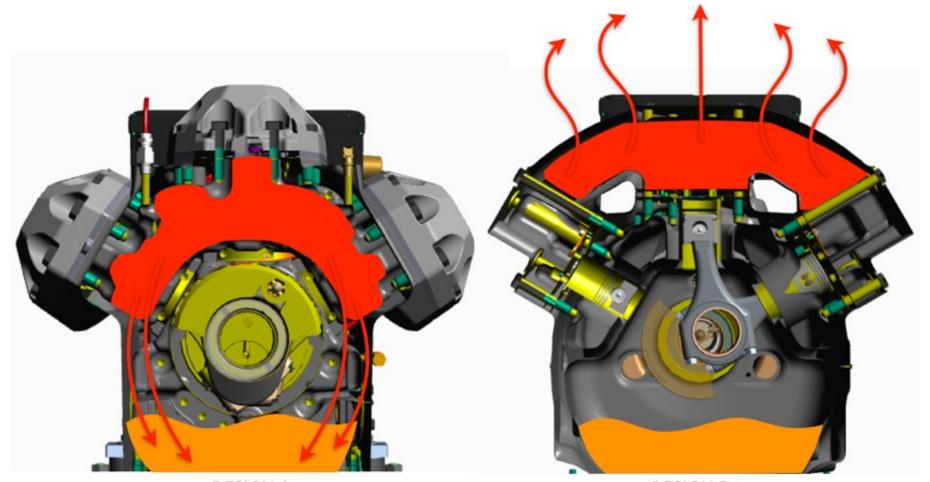


Figure 8. Interior view of a Design B - compressor with external discharge plenum

External Discharge Plenum:

- Open air circulation allows thermal insulation between HP and LP sides
- Lower heat dissipation towards the oil sump

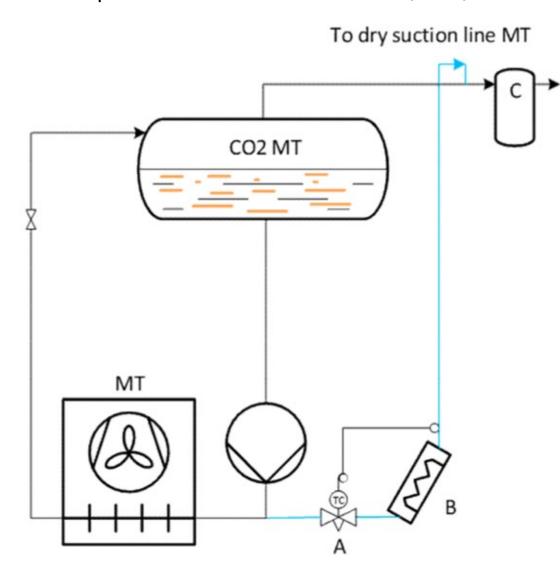
DESIGN A vs DESIGN B



DESIGN A:
COMPRESSION HEAT DISSIPATION TO OIL SUMP

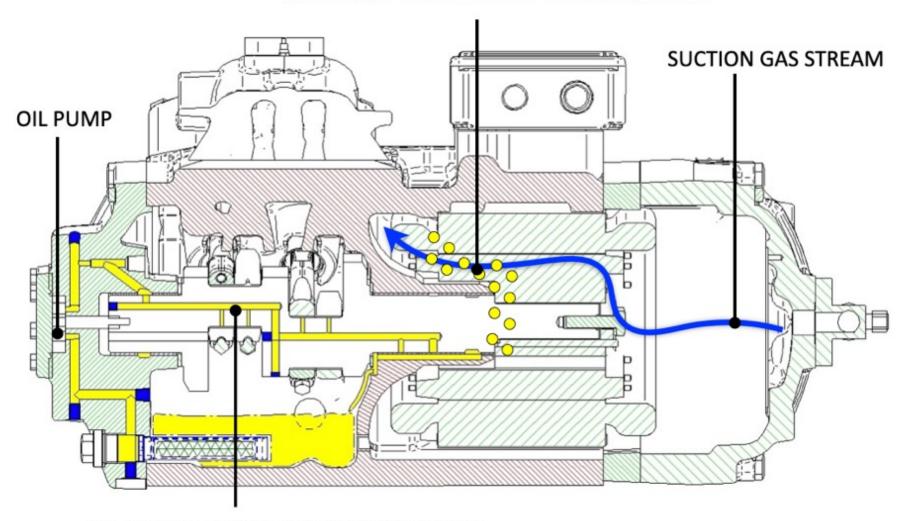
DESIGN B: COMPRESSION HEAT DISSIPATION TO SURROUNDING AMBIENT

Compressor Oil Circulation Rate (OCR)



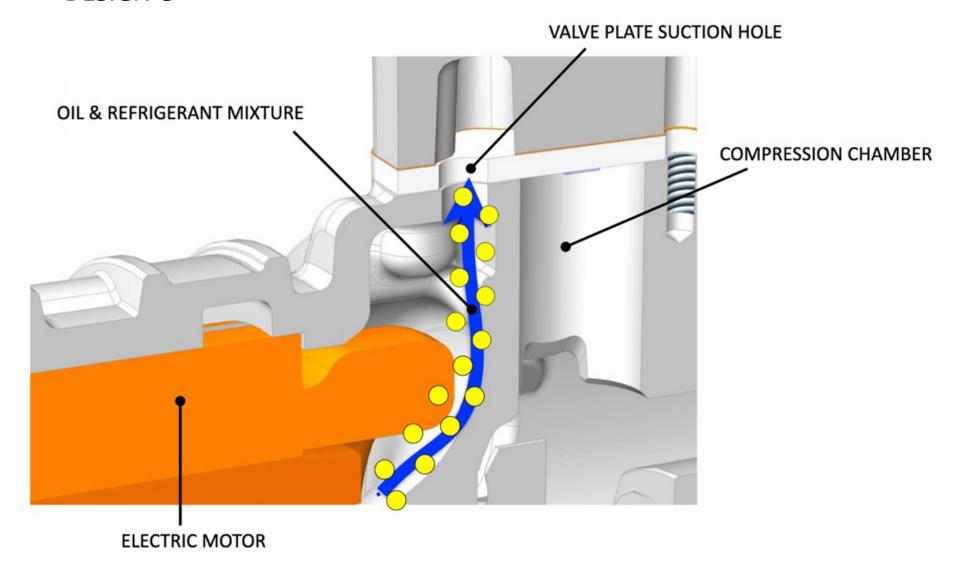
- Rectifier is triggered by low oil level into the reservoir.
- Pump energy is "wasted" to feed the rectifier.
- Liquid portion is bypassing the evaporator.

OIL EXITING THE LAST SUPPORT BEARING SET

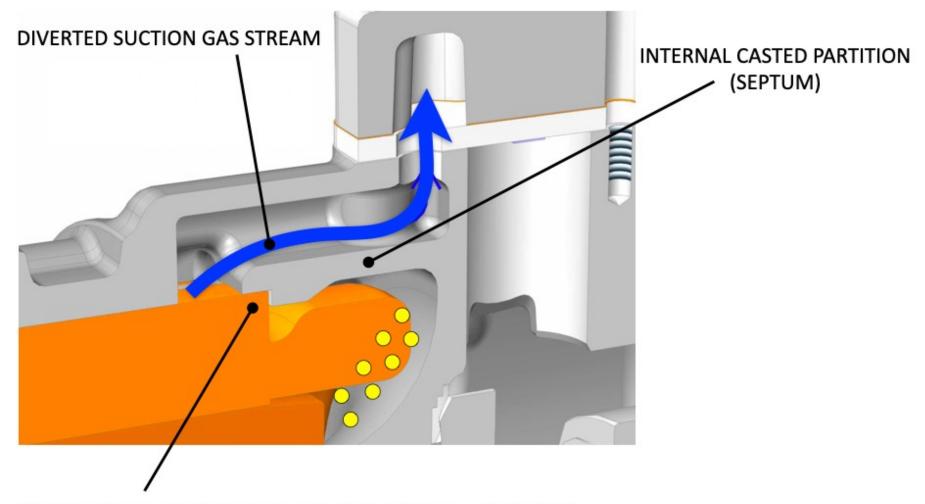


OIL STREAM THROUGH THE CRANKSHAFT

DESIGN C

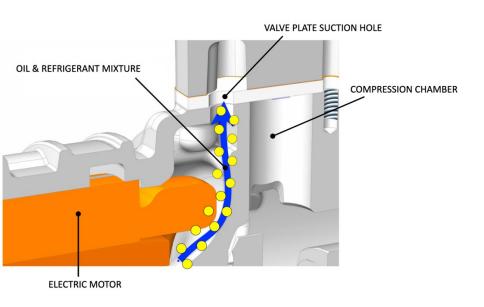


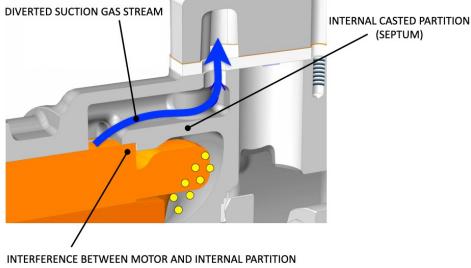
DESIGN D



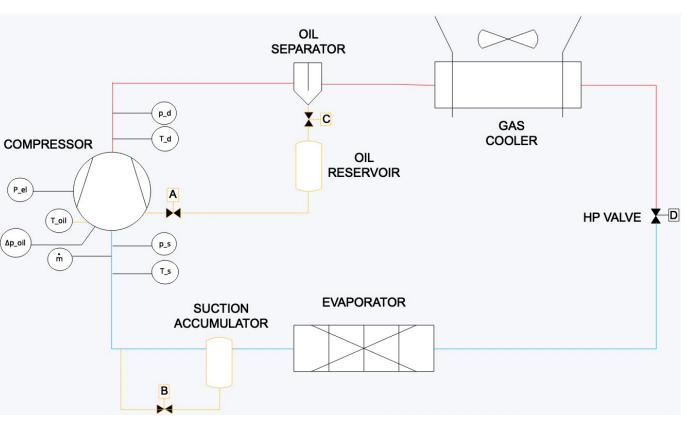
INTERFERENCE BETWEEN MOTOR AND INTERNAL PARTITION

DESIGN C vs DESIGN D





DESIGNS A – B – C – D have been tested in a CO2 Lab



p s: Suction Pressure

T_s: Suction Temp.

m: Refrigerant Mass Flow

Δp_oil: Oil Diff. Pressure

T oil: Oil Temp.

P_el: Power Consumption

HP VALVE ▼ p_d: Discharge Pressure

T_d: Discharge Temp.

*Valve A: allows compressor oil sump feed from oil reservoir

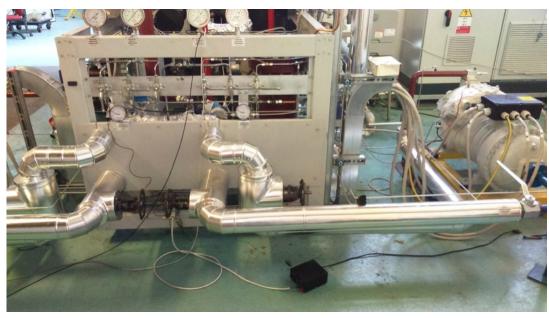
*Valve B: allows oil return from suction accumulator

*Valve C: ?

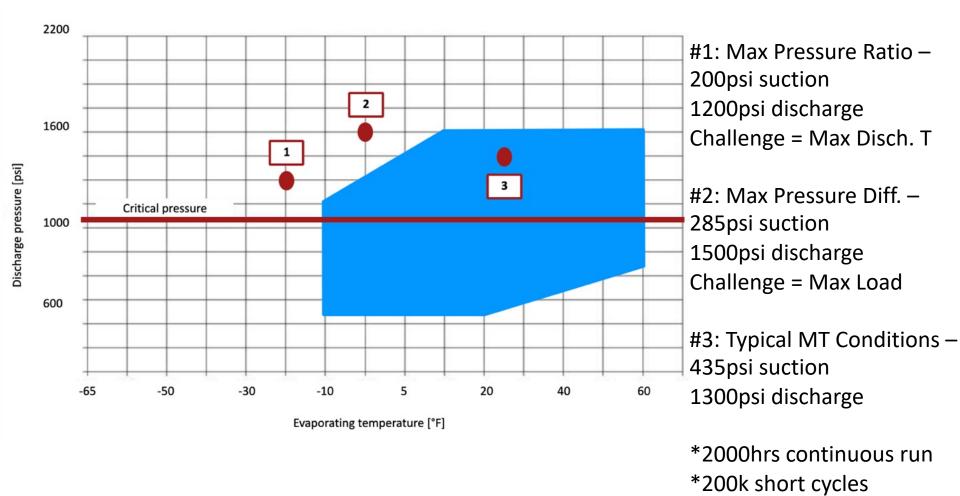
*Valve D:?



Gas Cooler

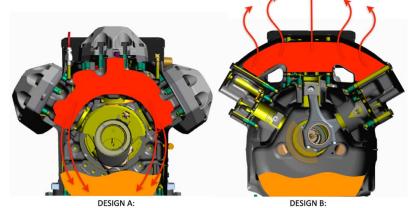


Compressor and Sensors Assembly



(5s on/5s off)

DESIGN A vs B: Performance & Reliability:



DESIGN A:
COMPRESSION HEAT DISSIPATION TO OIL SUMP

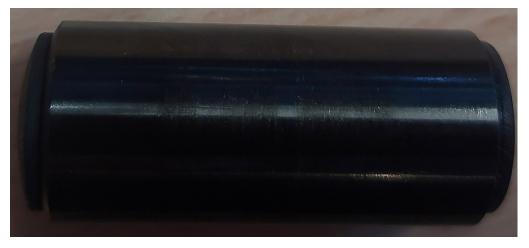
DESIGN B:
COMPRESSION HEAT DISSIPATION TO
SURROUNDING AMBIENT

TRANSCRITICAL COMPRESSORS TESTS: DISPLACEMENT 4412 cfh @ 60Hz							
reliability and performance	test	Design A			Design B		
p_s (suction pressure)	[psi]	200	285	435	200	285	435
p_d (discharge pressure)	[psi]	1200	1500	1300	1200	1500	1300
T_s (suction temperature)	[°F]	-4	14	40	-4	14	40
T_oil (oil temperaturee)	[°F]	167	158	155	125	118	113
T_d (discharge temperature)	[°F]	329	300	230	310	282	215
Oil Residual viscosity	[cSt]	13	10	9	25	22	16
m (mass flow)	[lb/h]	4857	7424	15905	5094	7751	16362
P_el (power consumption)	[kW]	116	143	165	112	138	161

DESIGN A vs B: Performance & Reliability:



A – Severe wear on wrist pin.



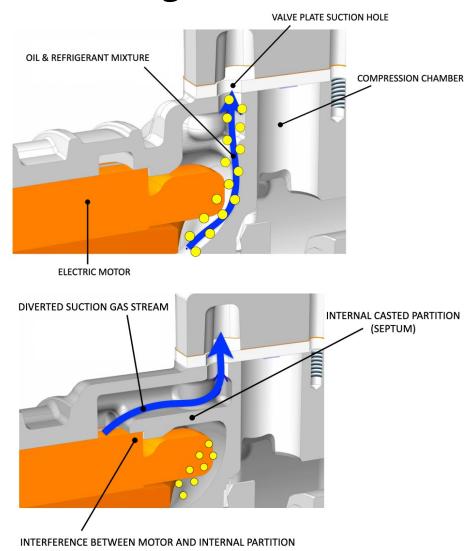
B – No wear on wrist pin.

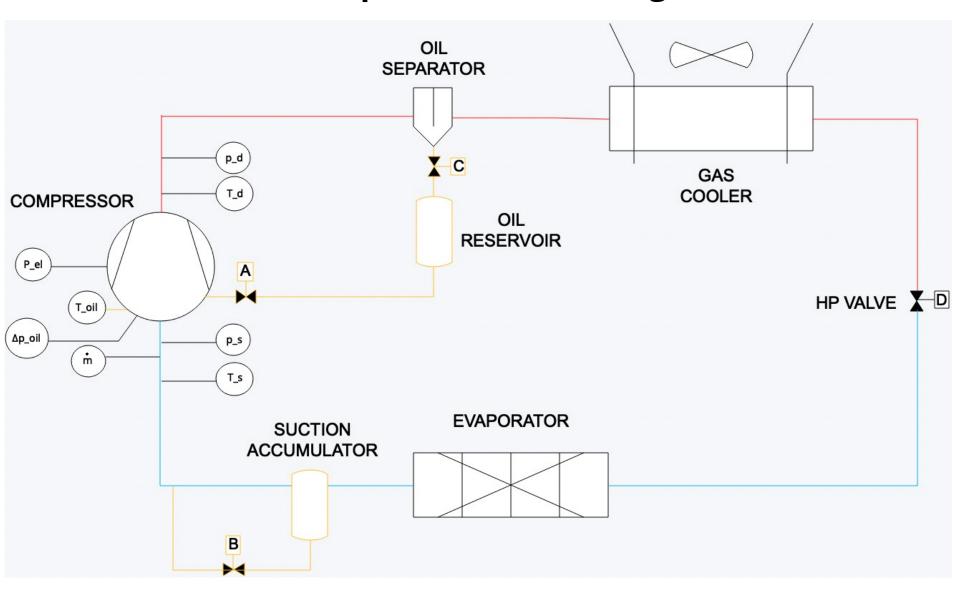
DESIGN C vs D: Oil Circulation Rate

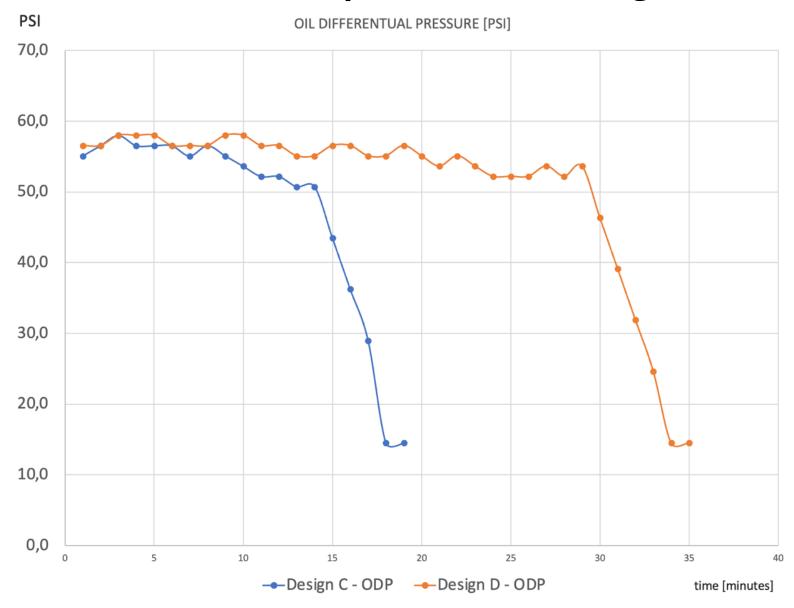
Test performed at typical MT conditions: 435psi suction / 1300psi discharge

Oil return ports closed, no oil return from system to the compressor.

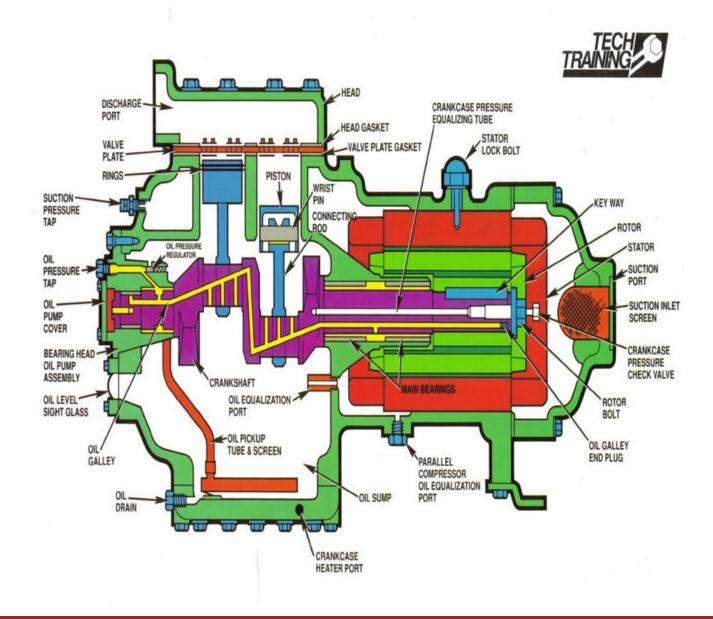
Oil differential pressure switch trigger time was measured and compared for both design C & D.



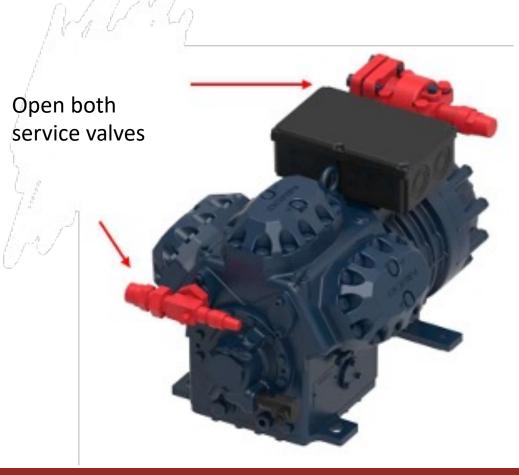




Parts of a Semi-Hermetic Compressor



 Before working on any compressor in the field, make sure to follow system instructions for turndown and proceed to isolate the compressor. After compressors are powered off and isolated, open both service valves to relieve pressure.



• Check the nameplate for information on the compressor:



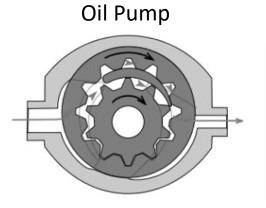
Max Load / Amp Draw

Oil

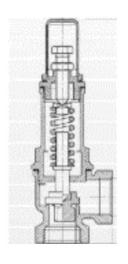
Safety Devices (varies by size of compressor):

LP / HP Relief Valve

Motor Protection







Electronic Protection Module



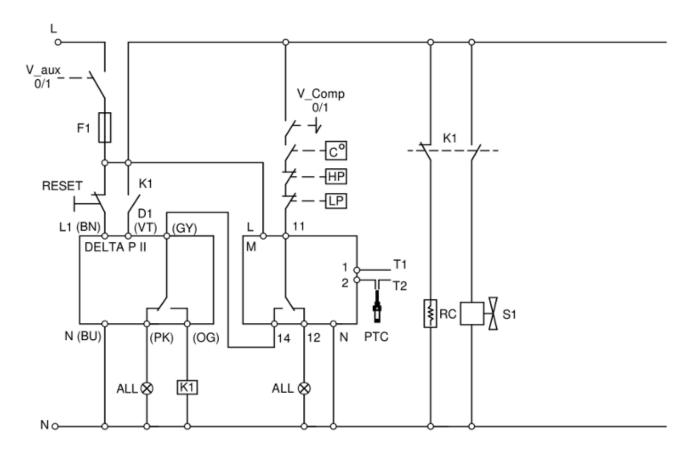
Max Discharge Temp. Sensor



Oil Differential Pressure Switch



Electrical Connection Scheme of Safety Devices:



V aux = Aux Power Supply V Comp = Compressor Power

F1 = Fuse

K1 = Contactor

RC = Crankcase Heater

S1 = Solenoid

M = Protection Module (INT69)

DELTA P II = Oil Diff. P Switch

HP = High Pressure Switch

LP = Low Pressure Switch

PTC = Discharge Temp. Sensor

1-2/T1-T2 = Thermistors

Diagnosing Compressor Failures

- Types of Mechanical Failures:
 - 1. Lubrication / Seizing
 - 2. Slugging
 - 3. Heat
 - 4. Contaminants



- 1. Single Phase
- 2. Burn Spots
- 3. Rotor Lock
- 4. Overload
- 5. PW Failure





 Lubrication / Seizing – Lack of lubrication will lead to a compressor seizing or locking up. During a teardown this will show up as dry-surfaces accompanying damage from seized part.

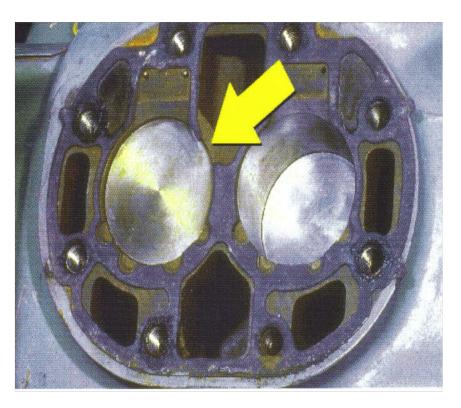






Prevention by making sure compressor has correct oil charge (~2/3 of sight glass) and there is no issue with oil returning to compressor.

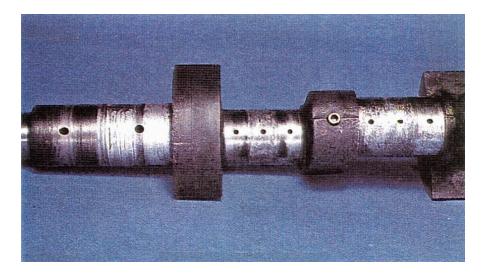
• Slugging – Typically top-end damage. Valves will be brittle and Cylinders/Valves will be dry.





Heat – Typically top-end damage. Discoloration will be present.





Caused by: Blow Gasket, Improper Head Gasket Install, Blown Discharge Valve, High Superheat, and Non-Condensables.

Prevention for technicians: Catch initial stages during check and install gaskets correctly.

Contaminants – Similar to heat symptoms but includes a sludge residue.







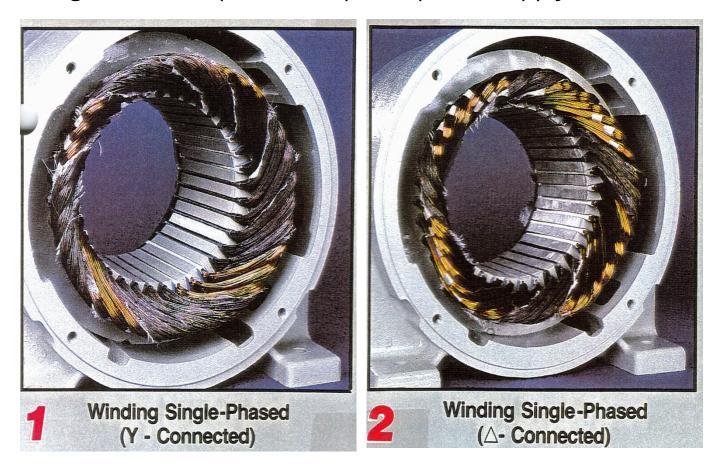
Caused by non-condensables (moisture, oxides, dirt, etc) that are introduced during improper oil change. Prevention would be to ensure clean oil and no contaminants are introduced during any repair work.

Electrical Failure – Confirmed by Motor Ohm Test

Motor Ohm Test - 5-40hp

Voltage 460 1.0 - 1.4 208 .35 208/230 .46 DV 37	L1-4 L2-5 L3-6	D Lead L7-8 L8-9 L9-7 Ground Check (L1-2 L2-3 L3-1 OK)	6 Lead L7-8 L8-9 L9-7 Open Check (3 Le L1-2 L2-3 L3-1	_
Overloads: Klixon: 06L's, 06D's, Etranes (except small motor) / Just want continuity Thermisters: M & R Tranes, JG/JS Yorks - ohm range below Copelands & Yorks - Kriwan - 50-80 ohm range / TI's on older motors 1100-1400 ohm range						
Tranes M & R's - Robert Shaw - 75 ohm range York - Kriwan 50-80 ohm range						
Common to: 1 _	2	3	Ground Chec	k (OK) (Open Check (OK)

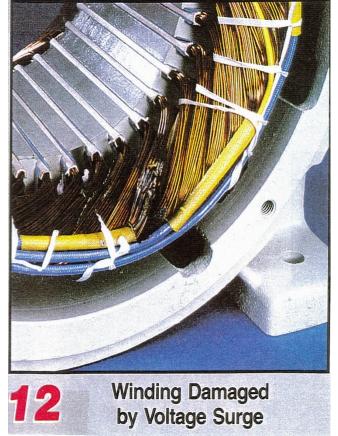
Single Phase – Open in one phase power supply to motor



Caused by blown fuse, open contactor on P/W Start, time delay for contactors, or bad connections. At this point, the you can only diagnose issue to prevent on replacement.

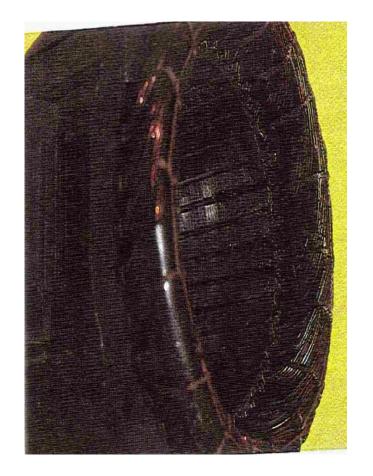
 Spot Burns – Developed due to chattering contactors or surge of power (lightning strike).





 Rotor Lock – Rotor rubs on stator and a short occurs. Caused by main bearing wear (lack of lubrication/heat).





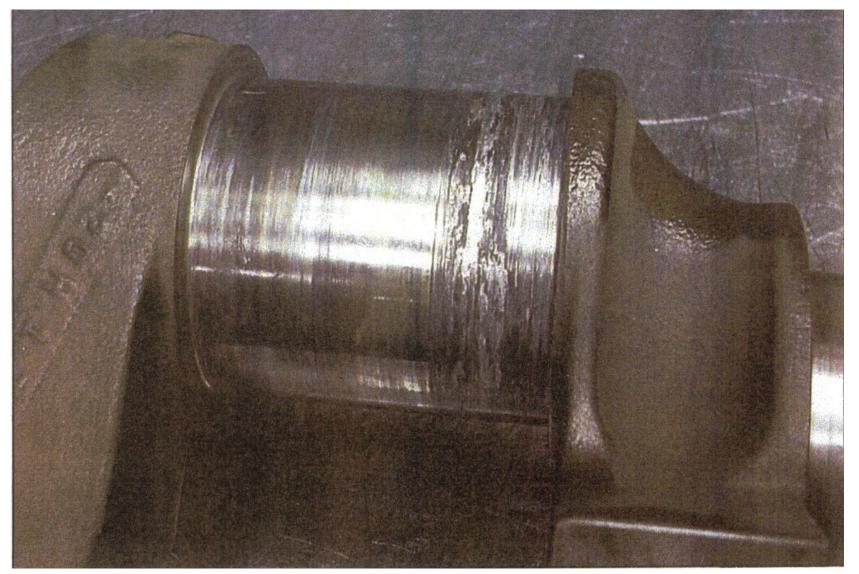
 Overload – Thermal deterioration of the insulation in all phases of the stator, typically caused by load exceeding rating of motor.



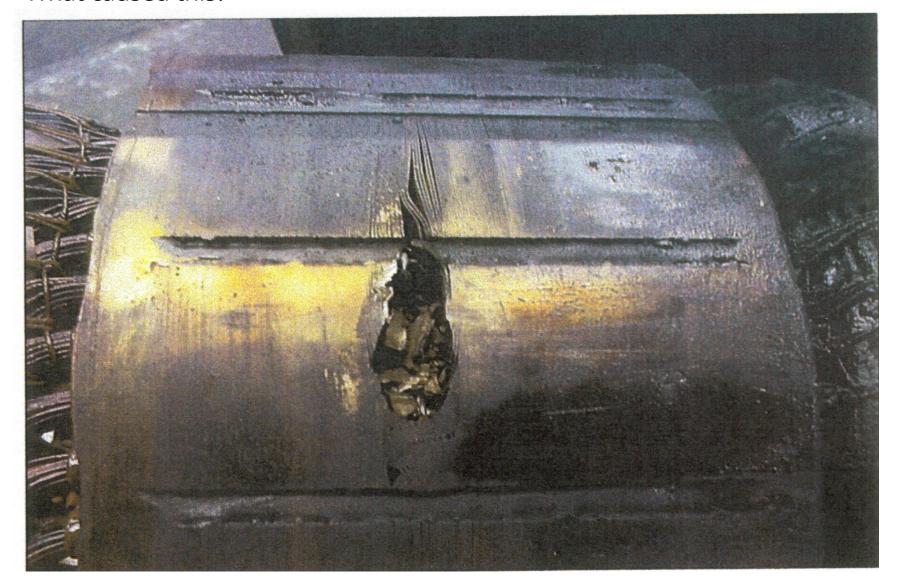
 Part Wind Failure – Caused by time delay between contactors or faulty operation of contactor. Prevented by dry-run of compressor.



• What caused this?



What caused this?



• What caused this?



Teardown of CO2 Compressor

We have brought a CO2 Compressor and will have a hands-on teardown.



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